

# **Toward Sustainable Chemicals and Fuels: Catalytic Conversion of Biomass Polyols to Olefins**

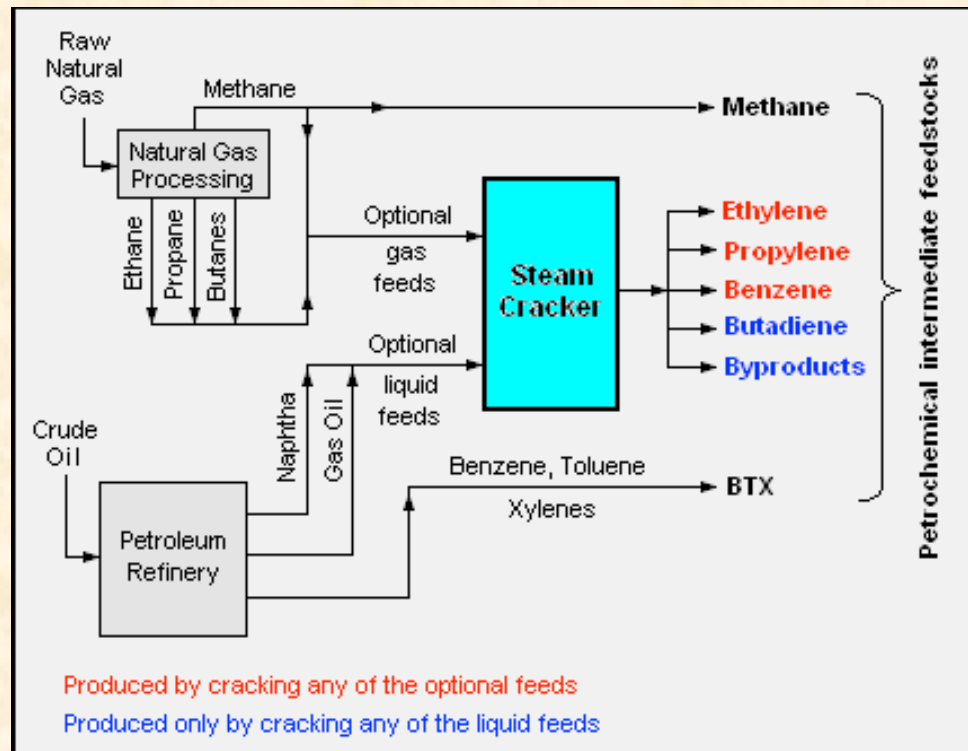
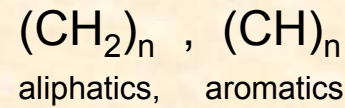
**Kenneth M. Nicholas**

**Department of Chemistry and Biochemistry**

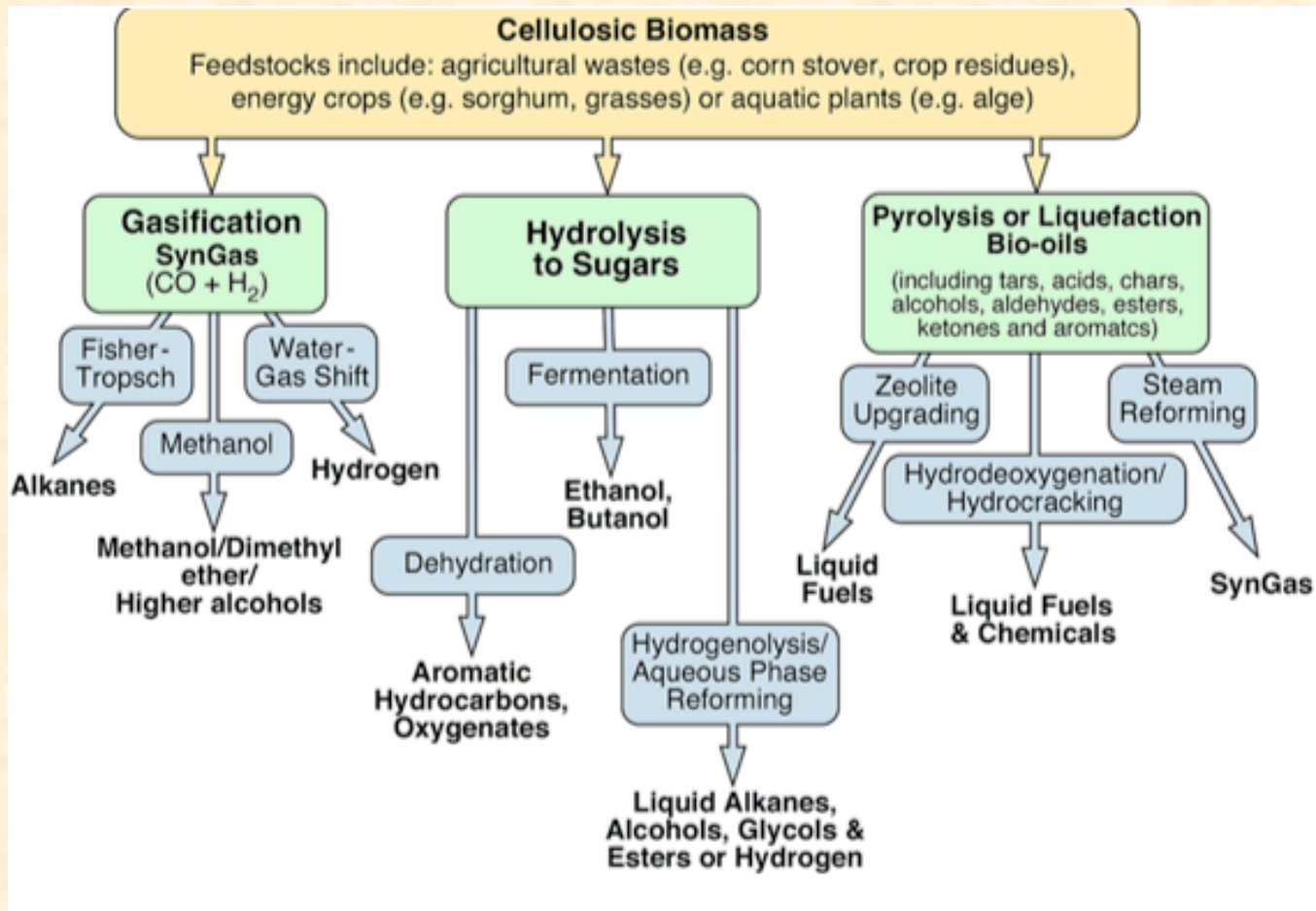
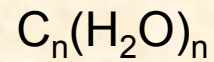




## Hydrocarbon Production from Fossil Resources

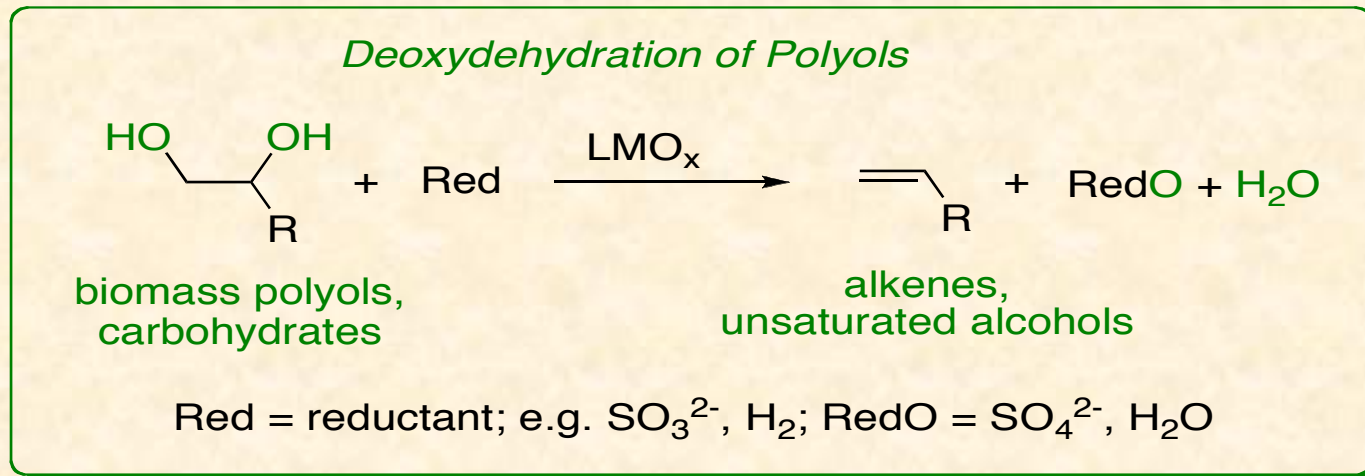


## Fuels and Chemicals from Cellulosic Biomass



## Deoxydehydration of Polyols (DODH)

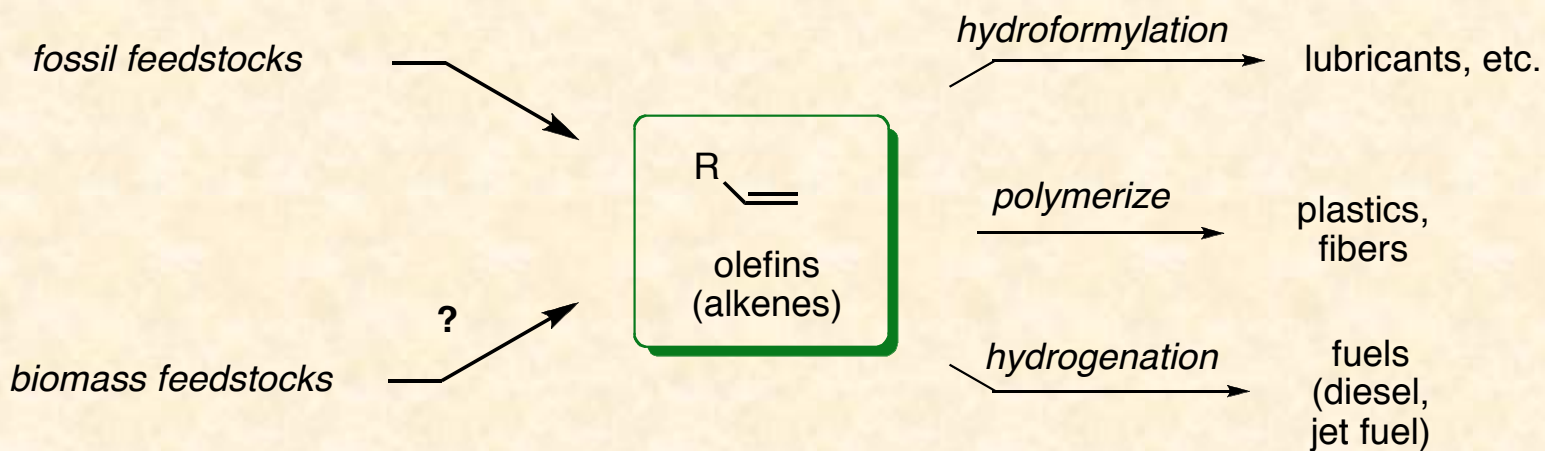
To convert abundant and renewable hydroxyl-rich biomass components into useful chemicals or fuels, selective processes are needed to remove some/all of the oxygens.



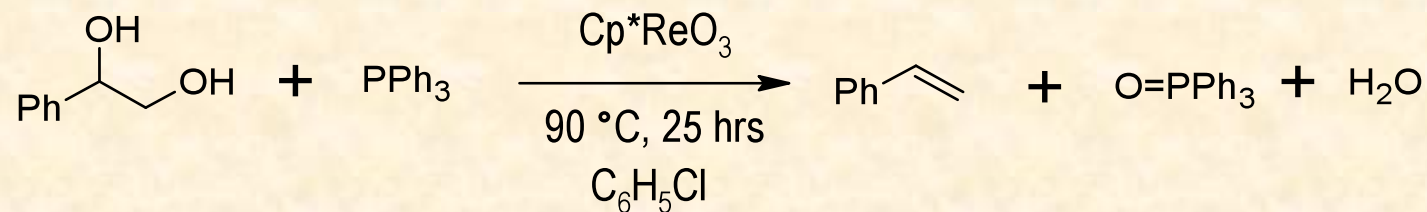
### *DODH features:*

- replaces 2 -OH with C=C
- requires a reducing agent (Red) and a catalyst
- produces higher energy, useful products
- requires selective -OH activation/removal by the catalyst

## Olefins are valuable chemical intermediates and products



## Prior/Recent Re-catalyzed DODH systems



G. Cook and M. Andrews, *J. Am. Chem. Soc.* **1996**, 118, 9448.

*Concurrent with our group's work:*

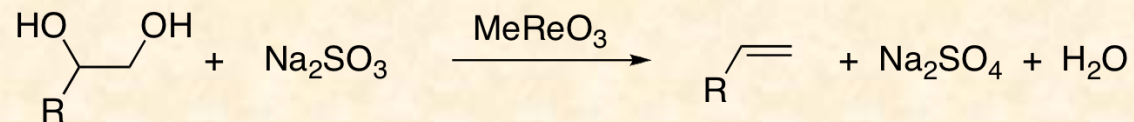
- $\text{MeReO}_3$  (cat) +  $\text{H}_2$  (RA)  
M. Abu-Omar et al. (Purdue), *Inorg. Chem.* **2009**, 48, 9998.
- $\text{Re}_2(\text{CO})_{10}$ /air + alcohol (RA)  
R.G. Bergman et al (U.C. Berkeley), *J. Am. Chem. Soc.* **2010**, 132, 11404.

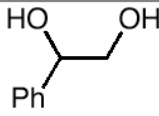
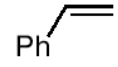
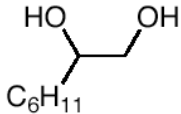
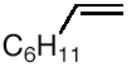
## Potential Reductants for Polyol DODH



<u>Reductant</u>	<u>Product</u>	<u><math>\Delta H^\circ</math> for DODH</u> <u>(kcal/mol)</u>	<u>Cost/mol</u>
<b>PPh<sub>3</sub></b>	<b>OPPh<sub>3</sub></b>	<b>- 17</b>	<b>\$ 5.0</b>
<b>H<sub>2</sub></b>	<b>H<sub>2</sub>O</b>	<b>- 14</b>	<b>\$ 0.01-.10</b>
<b>CO</b>	<b>CO<sub>2</sub></b>	<b>- 15</b>	<b>\$ 0.10-.50</b>
<b>Na<sub>2</sub>SO<sub>3</sub></b>	<b>Na<sub>2</sub>SO<sub>4</sub></b>	<b>- 13</b>	<b>\$ 0.10</b>

## MeReO<sub>3</sub> Catalyzes DODH by Sulfite Salts

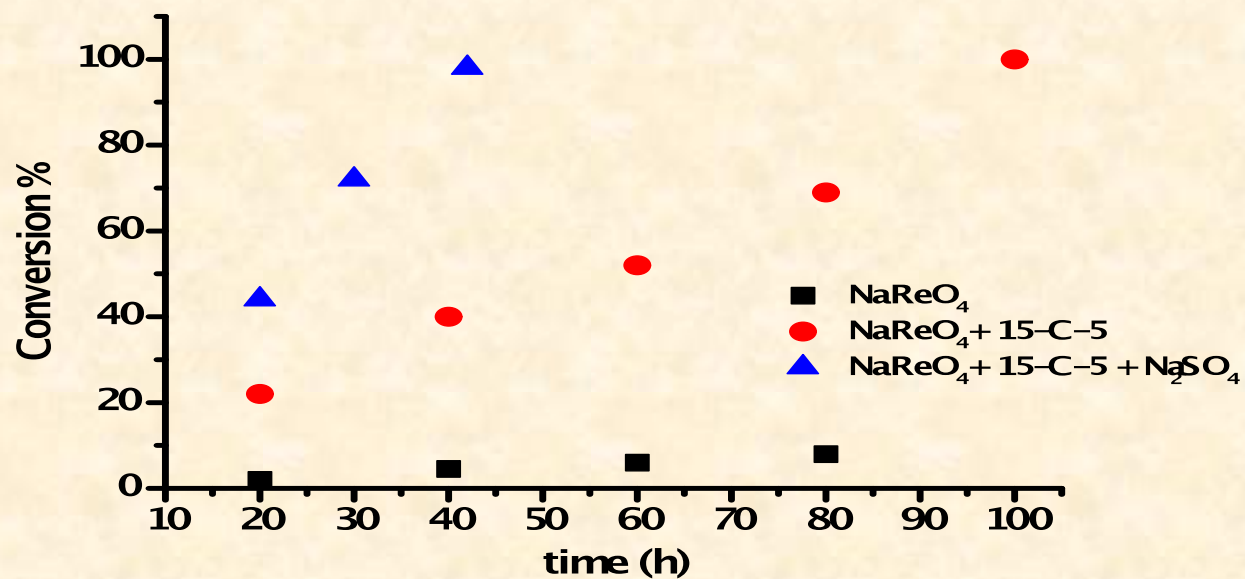
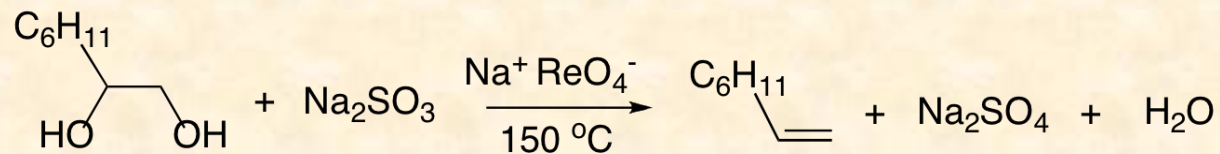


entry	substrate	Catalyst (mol%)	solvent/additive	major product	time (h)	% conv.	% yield <sup>a</sup>
1	 (0.2 M)	MeReO <sub>3</sub> (10)	benzene		4	100	59
2		(8)	benzene		4	100	59
3		(5)	THF		72	25	15
4		(5)	CH <sub>3</sub> CN		96	30	15
5		(8)	benzene		168	95	34
6		(8)	PhCl		40	100	45
7		(8)	PhCl, 15-crown-5		21	98	43
8		(2)	none		20	75	60

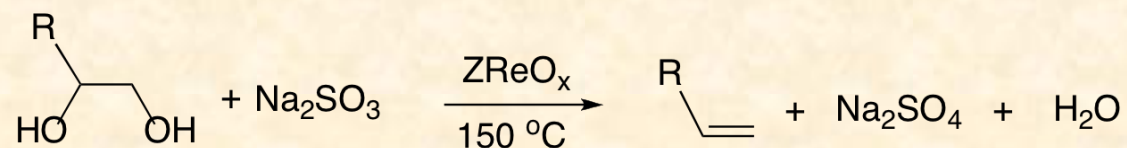
S. Vkuturi, G. Chapman, I. Ahmad, K.M. Nicholas, *Inorg. Chem.* **2010**, *49*, 4744.

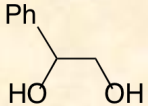

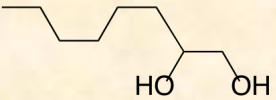
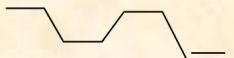


**Z<sup>+</sup> ReO<sub>4</sub><sup>-</sup> also catalyzes DODH;  
additives enhance conversion rate**

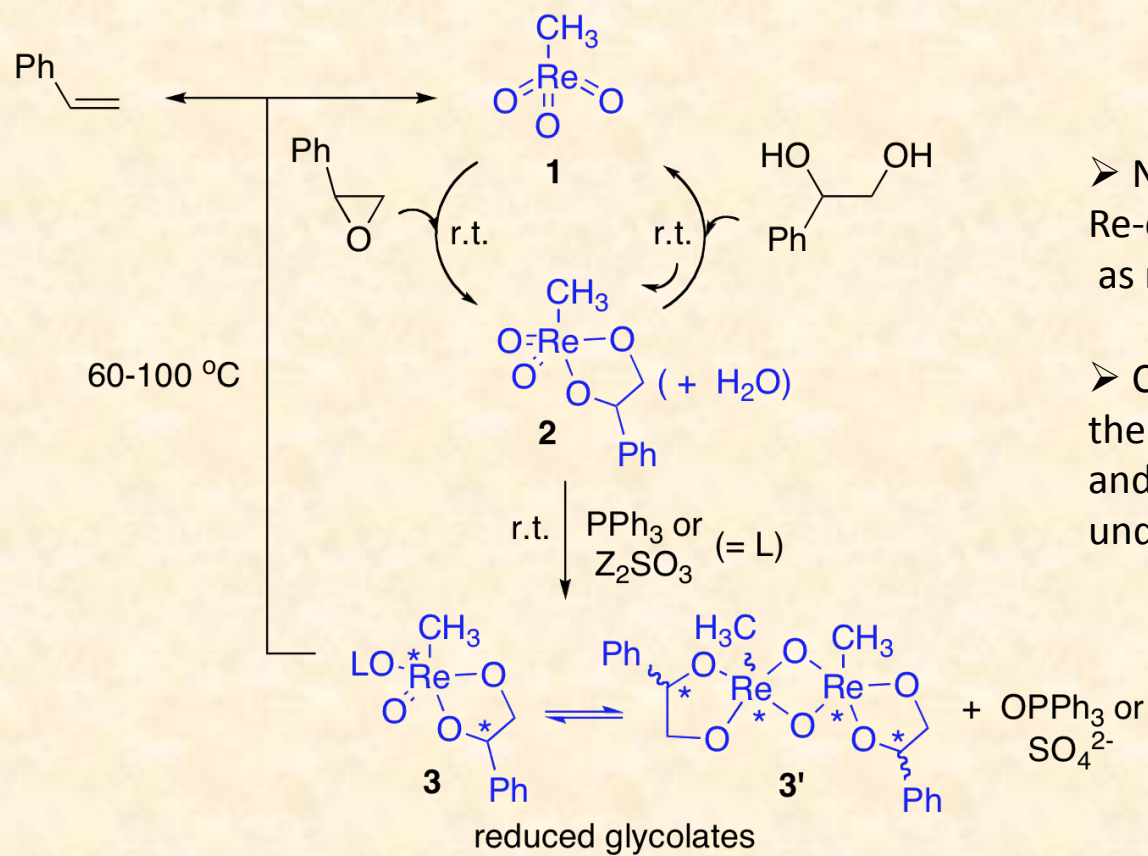


## Substrate, catalyst effects on $Z^+ReO_4^-$ DODH



Substrate	Catalyst	t (h)	Conv. <sup>b</sup> %	Yield %	Major product
	NaReO <sub>4</sub>	40	100	53	
	NH <sub>4</sub> ReO <sub>4</sub>	12	100	34	
	Bu <sub>4</sub> NReO <sub>4</sub>	59	100	71	
	Re <sub>2</sub> O <sub>7</sub>	63	80	23	
	NaReO <sub>4</sub>	42	98	38	
	NH <sub>4</sub> ReO <sub>4</sub>	26	100	37	
	Bu <sub>4</sub> NReO <sub>4</sub>	100	100	68	

## Detection of reactive intermediates



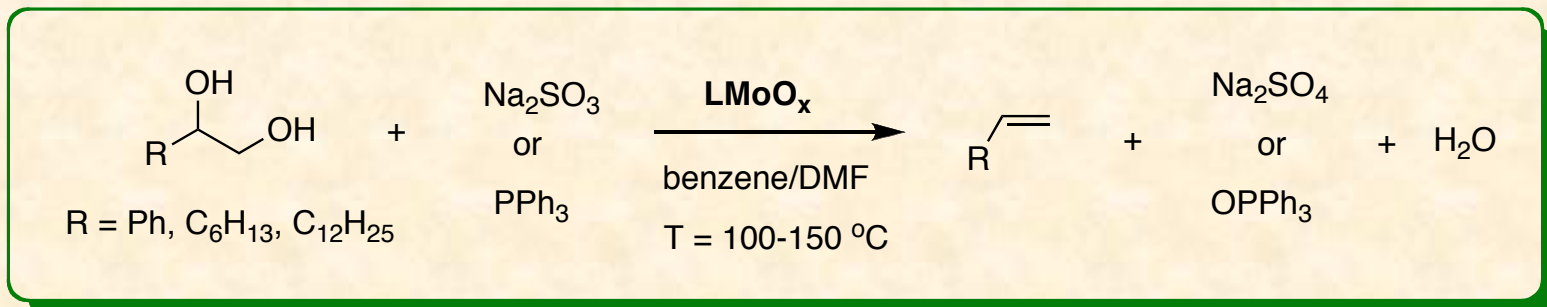
➤ NMR and IR studies detect Re-compounds **2** and **3** as reaction intermediates.

➤ Computational modeling of the reaction intermediates and transition states is underway.

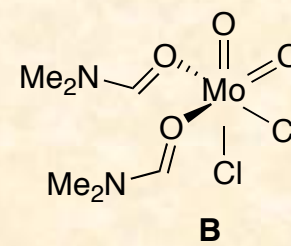
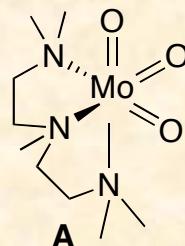
I. Ahmad, G. Chapman, K.M. Nicholas, *Organometallics*, **2011**, 30, 2810.



## Toward cheaper, more efficient catalysts: Molybdenum



$\text{LMO}_x = (\text{NH}_4)_6\text{Mo}_7\text{O}_{24}, (\text{Bu}_4\text{N})_2[\text{Mo}_6\text{O}_{19}], (\text{Bu}_4\text{N})_3[\text{Mo}_{12}\text{O}_{40}]$ ,

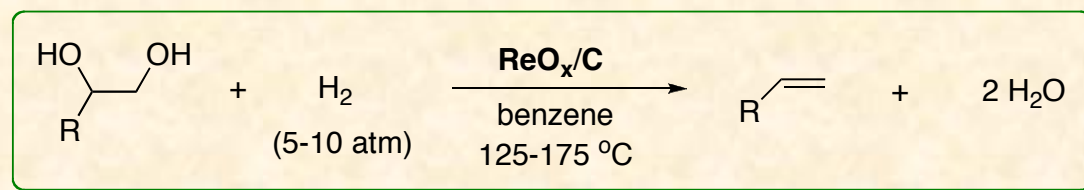
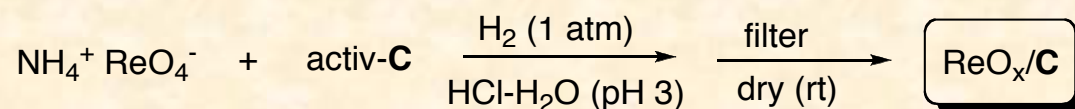


Catalyst (mol%)	Reductant (mmol)	Temp. (°C)	Time (h)	Conversion (% approx)	Alkene Yield (%)
$(\text{NH}_4)_6\text{Mo}_7\text{O}_{24}$ (10)	Sulfite	150	53	85	18
$\text{MoO}_2\text{Cl}_2(\text{DMF})_2$ (3)	Sulfite	150	24	100	17
$(\text{NH}_4)_6\text{Mo}_7\text{O}_{24}$ (10)	$\text{PPh}_3$	150	48	100	30
$\text{MoO}_2\text{Cl}_2(\text{DMF})_2$ (3)	$\text{PPh}_3$	100	3	100	33

Dr. Sanjeev Maradur, 2012.

## Toward practical *heterogeneous* DODH catalysts

A joint-project with F. Jentoft (O.U. CBME) provides a proof-of-concept:



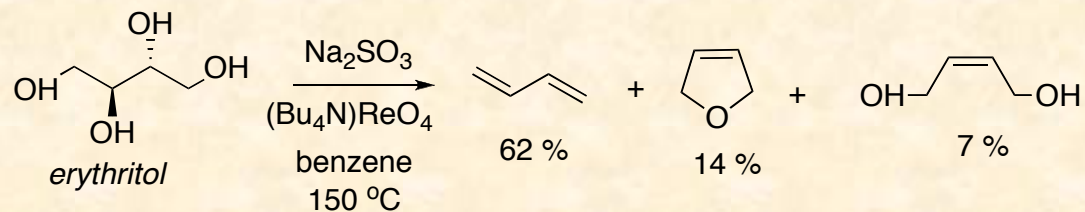
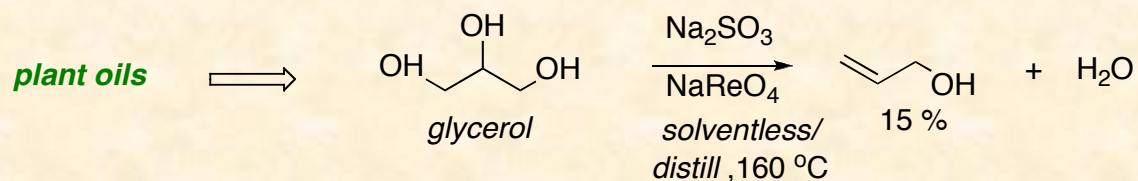
Catalyst	Time (hr)	Tetradecene (%)
fresh (4 % Re)	25	12
	48	23
	72	42
filtrate + glycol	72	43

➤ little/no alkane formed

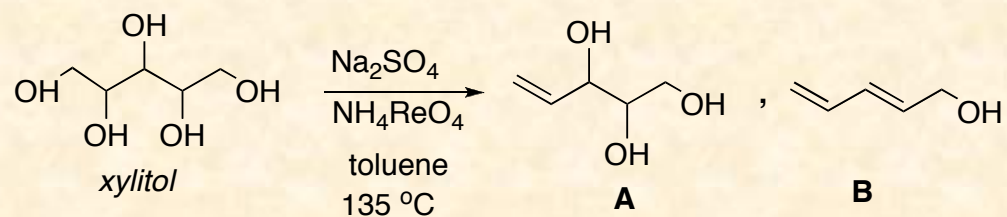
➤ catalyst recycling shows 50% decrease in activity after 4 reuses



## Biomass feedstocks to value-added products



*cellulose, sugars*  $\Rightarrow$



1:1 Xyl/SO<sub>3</sub><sup>2-</sup> A (20 % yield) >> B

1:2 Xyl/SO<sub>3</sub><sup>2-</sup> B (40 % yield) >> A

Dr. Irshad Ahmad (2011), Camille-Boucher-Jacobs (2012)

## Acknowledgements: People





## **ACKNOWLEDGEMENTS: \$\$\$**

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